

## Numerical Investigation of fluid flow Over a Lid-driven Square Cavity

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### ABSTRACT

This work is focused on numeric investigation of fluid flow over a lid-driven cavity. A square cavity is chosen to do the simulation. The simulation is done for both laminar, transient and turbulent flow for both 2D and 3D case. Reynolds number is considered between  $1 < Re < 7500$ . First the mesh independence test is done by different mesh size. Five different quadratic mesh configuration is used for mesh independence test. Finally a  $200 \times 200$  cell elements are used for the final simulation. Commercial software ANSYS Fluent is used for the simulation. A pressured based solver is used with QUICK solution schema to find the horizontal velocity components at different Reynolds number. The results are compared with available published data. There are significant agreement with the experimental data. Streamlines at different Reynolds number, position of the primary and secondary vortex are compared with the experimental data and presented.

Keywords: lid driven cavity, vortex, CFD

### 1. Introduction

Flow through a lid driven cavity is one of the classic fluid mechanics problem used for validation and verification of fluid flow models. Due to the simplicity of the geometry and complex flow field, this problem has been used for verification of 2D Navier Stokes equation as it is very difficult to capture the flow phenomena near the singular points near the corner of the cavity [1-2]. The cavity analysis is used for material process, metal casting, designing journal bearing and many more.

Many researcher have done significant amount of work on cavity flow. Ghia et al [3] have done the detail analysis of cavity flow. N.A.C Sidik et al [4] considered the cubic interpolated pseudo particle method validate their results with shear driven flow in shallow cavity. There have been some works devoted to the issue of heat transfer in the shear driven cavity. Manca et al [5] presented a numerical analysis of laminar mixed convection in an open cavity with a heated wall bounded by a horizontally insulated plate. Results were reported for Reynolds numbers from 100 to 1000 and aspect ratio in the ranges from 0.1 to 1.5. They presented that the maximum decrease in temperature was occurred at higher Reynolds. The effect of the ratio of channel height to the cavity height was found to be played a significant role on streamlines and isotherm patterns for different heating configurations. The investigation also indicates that opposing forced flow configuration has the highest thermal performance, in terms of both maximum temperature and average Nusselt number. Numerical simulation of unsteady mixed convection in a driven cavity using an externally excited sliding lid is conducted by Khanafer et al [6]. They observed that,  $Re$  and  $Gr$  would either enhance or retard the energy

transport process and drag force behavior depending on the conduct of the velocity cycle.

Ch.-H. Bruneau and M. Saad [7] have pointed out that, driven cavity flows exhibit almost all the phenomena that can possibly occur in incompressible flows: eddies, secondary flows, complex three-dimensional patterns, chaotic particle motions, instability, and turbulence. Thus, these broad spectra of features make the cavity flows overwhelmingly attractive for examining the computational schemes.

### 2. Objective

The purpose of the study is to investigate the flow behavior through the lid-driven cavity and to calculate flow separation and recirculation zone at different  $Re$ . In order to validate the result, the simulated data would have to compare with the experimental data [1].

### 3. Theory

The simulation is done by solving 2D Navier-Stoke equation for constant density flow. The continuity and momentum equation for a steady state 2D constant density flow are given as follows-

Continuity Equation,

$$\frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} = 0$$

For Constant density,

$$\rho \left( u \frac{\partial u}{\partial x} + v \frac{\partial u}{\partial y} \right) = \mu \left( \frac{\partial^2 u}{\partial x^2} + \frac{\partial^2 u}{\partial y^2} \right) + \rho g_x$$



boundary condition is determined based on Re. For Re calculation the characteristic length is assumed as L, where L is the depth.



Standard least square discretization technique is used. A second order upwind solution method with QUICK solver is used. Re is set from 1 to 5000 as inlet condition. For convergence, the residue for continuity and velocity is set as 1e-10. Each solution is allowed to run 10,000 iteration to meet the minimum convergence criteria. To validate the CFD model, u-velocity is at  $x=0.5L$  and  $Re = 400$  is compared with the published data. Figure 4 shows the comparison of CFD results which have a good agreement with experimental data.

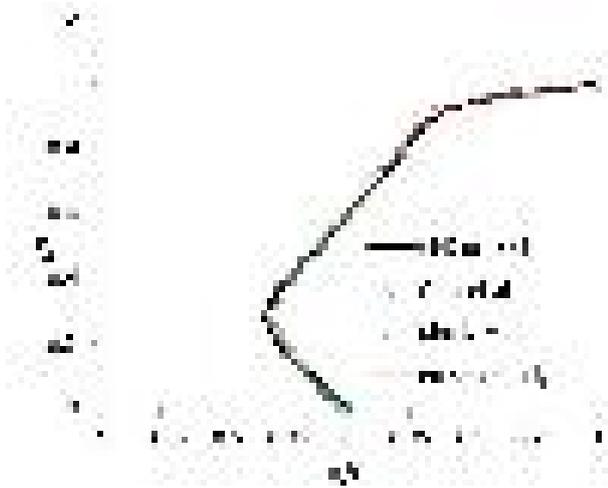


Figure 4. Validation of result at  $x = 0.5L$  and  $Re=400$

## 6. Results and Discussion

Horizontal velocity have been calculated for different Re ranging from 100 to 5000 in order to observe the flow behavior in Laminar, transition and turbulent regimes. The primary vortex form initially and as Re increases the vortex change its position. Figure 5 shows a typical streamline to demonstrate the formation of primary, secondary and tertiary vortex. Table 1 shows the center position of the primary vortex at different Re. It also shows the published data. The results are significantly close enough. Figure 6 shows the x-y coordinates of the primary vortex. It also shows the deviation from the published result. It is observed that, the center of the primary vortex become close to the center of the cavity as Re increases.

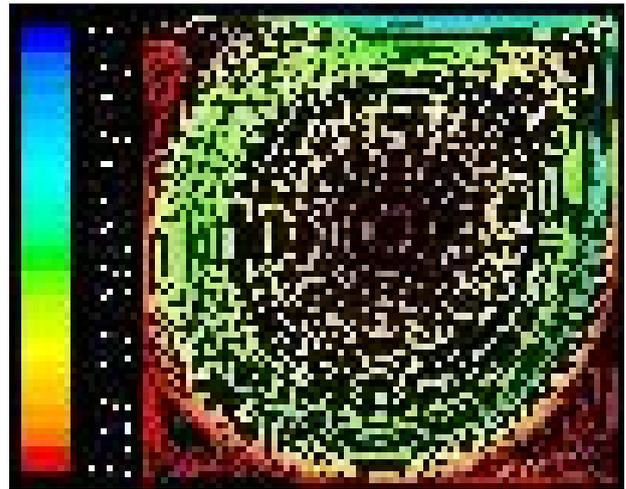


Figure 5. Different vortex formation at  $Re = 5000$

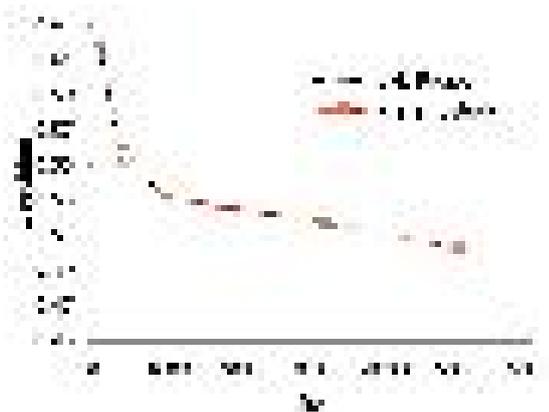
Table 1. Position of the center of the primary vortex

Re	100	400	1000	3200	5000
<b>Present</b>	(0.6 19,0. 742) 21 * 21	(0.560, 0.607) 31 * 31	(0.532, 0.564) 41 * 41	(0.518, 0.540) 61 * 61	(0.50 2, 0.514 ) 61 * 61
<b>Ghia 82</b>	(0.6 17, 0.73 4) 129 * 129	(0.555, 0.606) 257 * 257	(0.537, x) 257 * 257	(x , 0.547) 257 * 257	(0.51 2, 0.535 ) 257 * 257
<b>CFD Project</b>	(0.6 14, 0.73 4) 250 * 250	(0.553, 0.606) 250 * 250	(0.532, 0.562) 250 * 250	(0.540, 0.518) 250 * 250	(0.53 5, 0.502 ) 250 * 250



Figure 6. Coordinate of primary vortex at different Re

Figure 7(a) and 7(b) also show the change of position of the primary vortex in X and Y coordinate. The results are also compared with the published data and the deviation is significantly low. Figure 8(a) - 8(g) shows the streamlines at different Re. The primary and the secondary vortices are clearly visible there. The simulation successfully resolved the tertiary vortex at the corner of the cavity at Re = 5000 showed in figure 8(g).

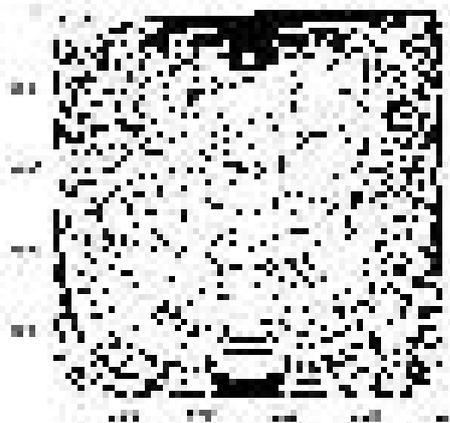


7(a)

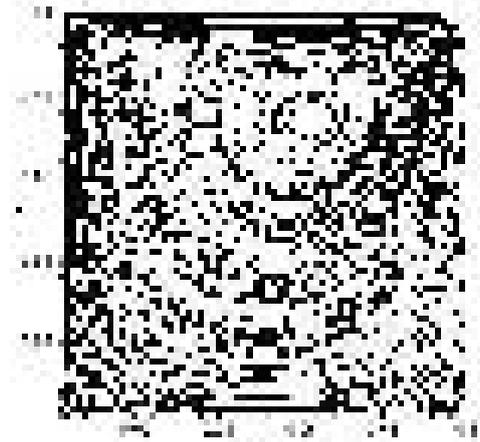


7(b)

**Figure 7.** Position of the primary vortex at different Re. (a) X-coordinate, (b) Y - coordinate



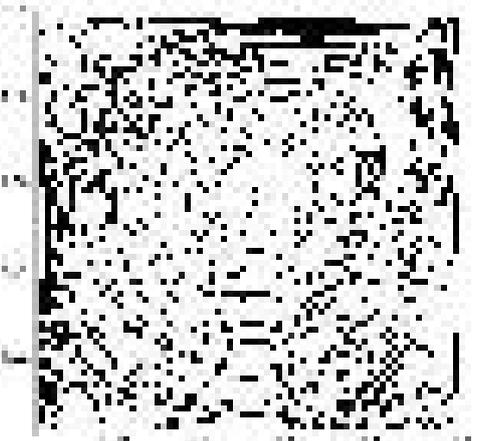
8(a) Re = 1



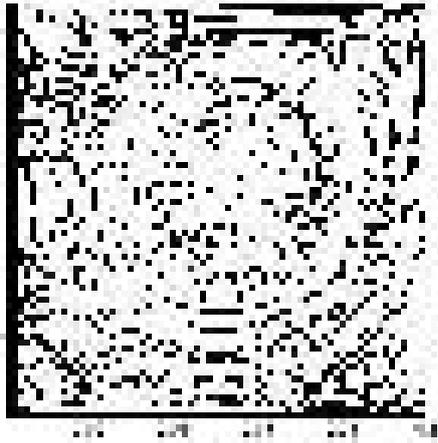
8(b) Re = 100



8(c) R = 400



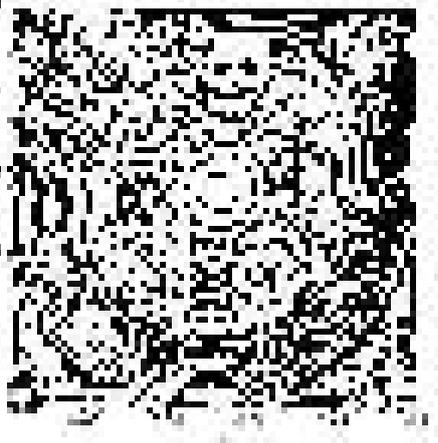
8(d) Re = 1000



8(e) Re = 2000



8(f) Re = 3200



8(f) Re = 5000

A 3D flow simulation is also done for the cavity. Figure 9 shows the velocity contour at the center of the cavity. Figure 10 shows the volumetric streamline for the cavity. The streamline is showed with particle form.

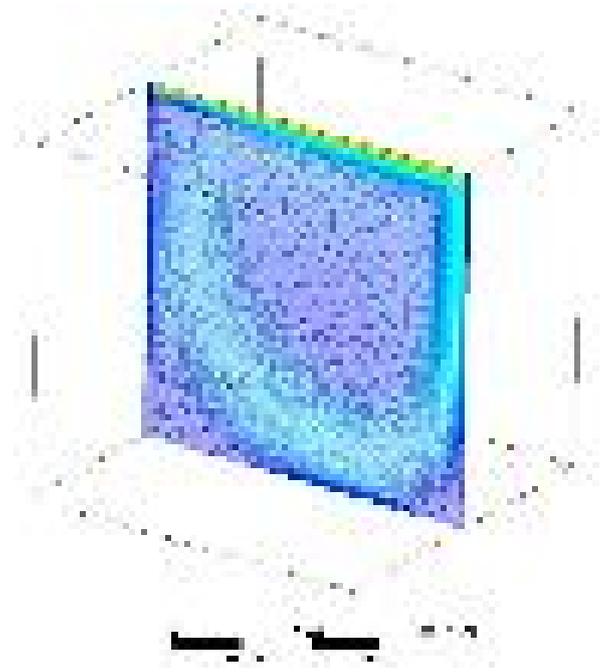


Figure 9. Velocity contour at the center plane of the cavity at Re = 400

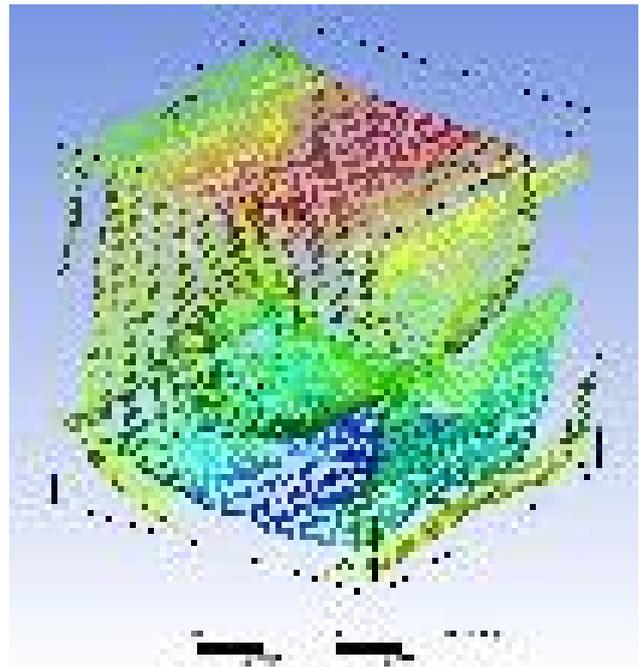


Figure 10. Streamline in particle form at Re = 400

## 7. Conclusion

The flow through a square cavity is simulated for both 2D and 3D case for different Re and the position of the vortices are presented. Mesh dependency is done for different cell number. The results are compared with the published data and it shows good agreement with published work.

## NOMENCLATURE

$u$  = Dimensional velocity component  
 $v$  = Dimensional velocity component  
 $U_0$  = Top wall's velocity  
 $T$  = Temperature  
 $U_0, U_0', U_0''$  = Secondary velocity  
 $U^*$  = Dimensionless velocity  
 $v^*$  = Dimensionless velocity  
 $T^*$  = Dimensionless temperature  
 $\mu$  = Dynamic viscosity  
 $\rho$  = Density  
 $\nu$  = Kinematic viscosity  
 $\gamma$  = Dimensionless velocity

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